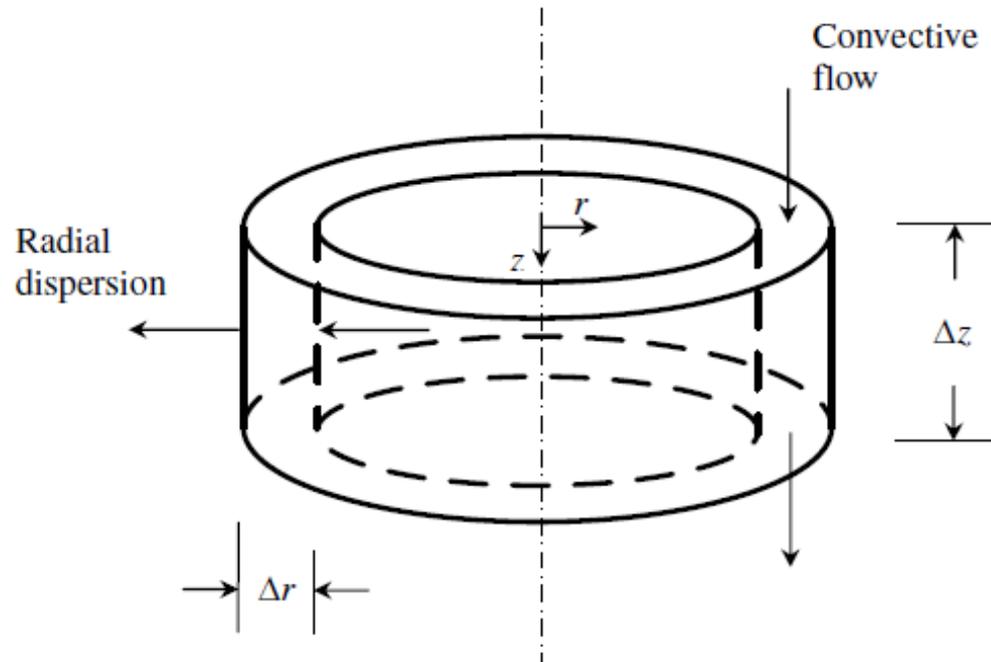


# CHE 611

# Advanced Chemical Reaction Engineering



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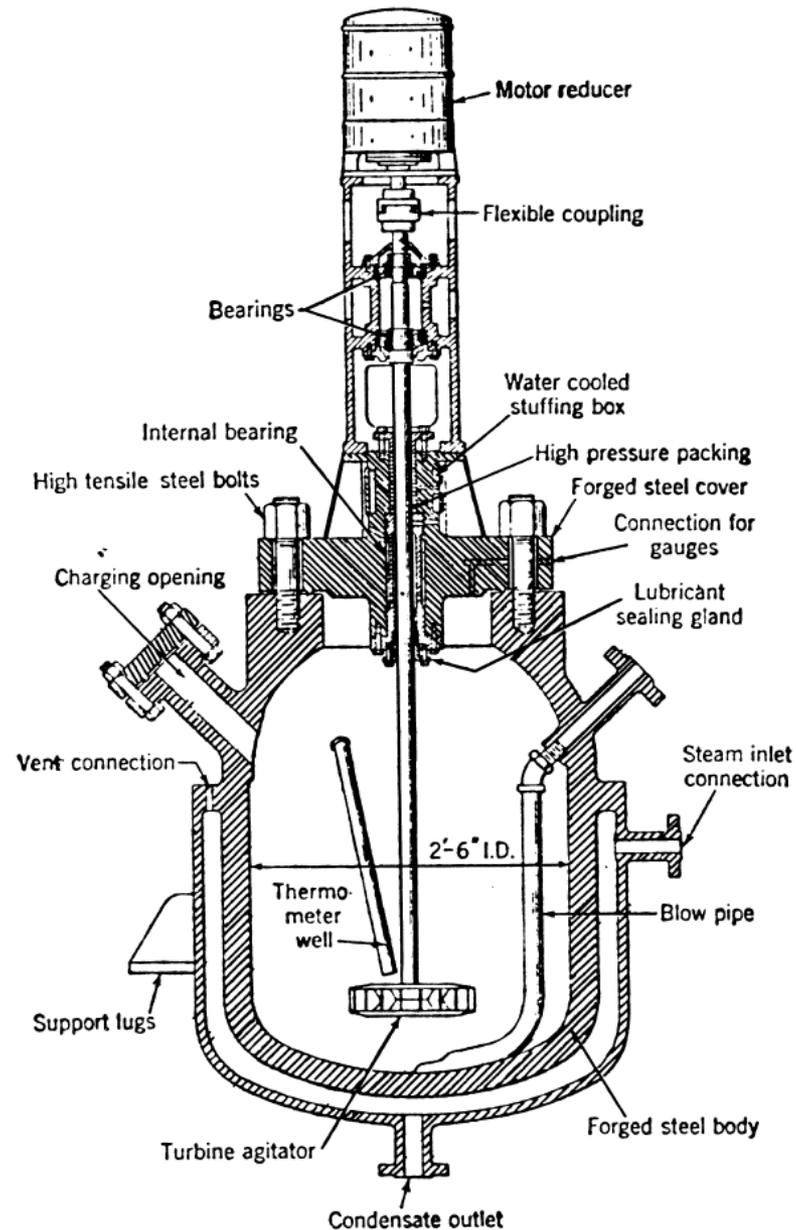
[mrusman.icet@pu.edu.pk](mailto:mrusman.icet@pu.edu.pk)

# **Advanced Chemical Reaction Engineering**

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## **Reactor Types**

# An example Batch Reactor [p.602, 13]



# Designs of reactors

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Based on the phases involved, reactors may adopt various shapes and designs depending upon the process requirements.

**What is a phase?**

# Reactors for gas phase only<sup>[15]</sup>

- If rate of the reaction is high, the reaction can be carried out in small reaction spaces e.g. in flames and arcs.
- For slower reaction larger reaction space is required.

Flame



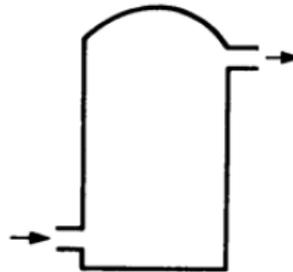
Examples:  
combustion of  
chlorine  
detonating  
gas, dissociation  
of methane

Electric arc



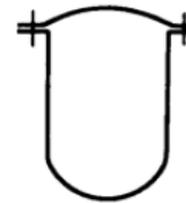
Examples:  
acetylene  
from methane,  
combustion  
of nitrogen

Large reaction  
vessel



Example:  
nitrogen  
oxidation

Autoclave



Example  
(laboratory):  
acetylene  
decomposition  
to acetylene  
black

Reaction engine

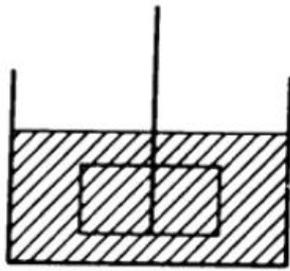


Example  
(laboratory):  
combustion of  
chlorine  
detonating  
gas

# Reactors for liquid phase only<sup>[15]</sup>

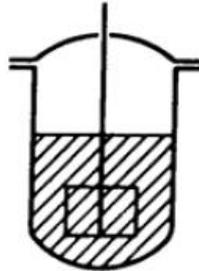
- Batch operations are common.

Tank



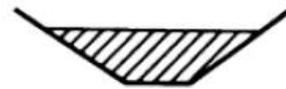
Examples:  
diazotization,  
dye coupling,  
potash recovery,  
benzene refining

Autoclave



Example:  
numerous  
organic  
processes

Crucible



Examples:  
glass melting,  
Siemens-Martin  
furnace

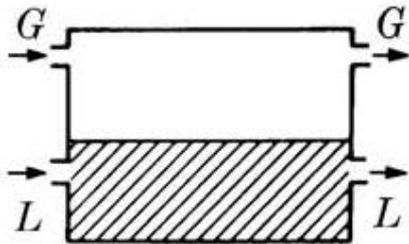
Vat



Example:  
glass melting

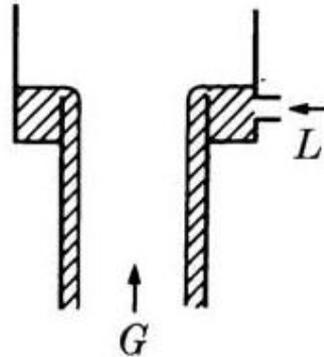
# Gas-liquid reactors<sup>[15]</sup>

Surface contactor



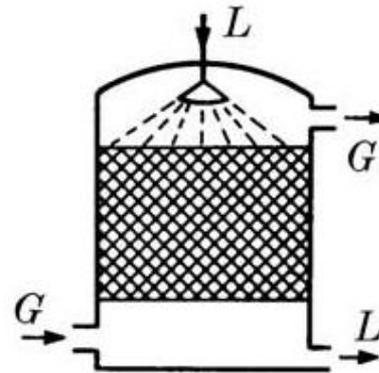
Example:  
HCl absorption

Wetted-wall absorber



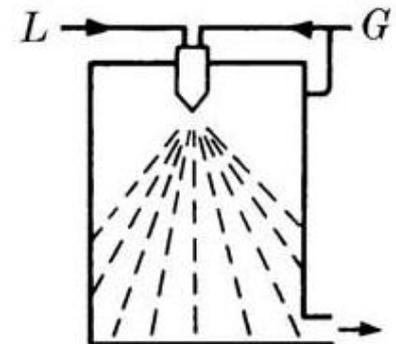
Example:  
HCl absorption  
in carbon  
tubes

Packed-bed reactor



Example:  
manufacture  
of HCl, H<sub>2</sub>SO<sub>4</sub>,  
and HNO<sub>3</sub>

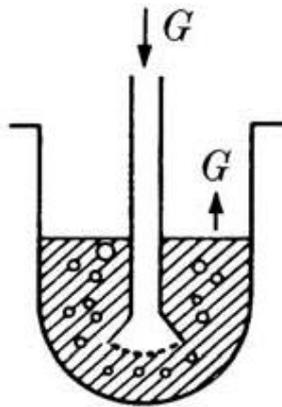
Spray reactor



Example:  
manufacture  
of phosphoric  
acid

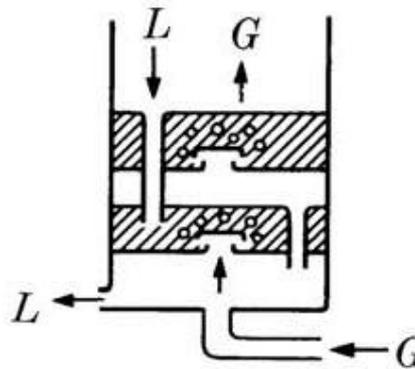
# Gas-liquid reactors<sup>[15]</sup>

Submerged bell



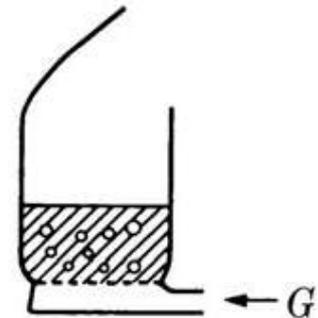
Example:  
 $\text{CO}_2$  scrubbing

Bubble-cap column



Example:  
HCl absorption

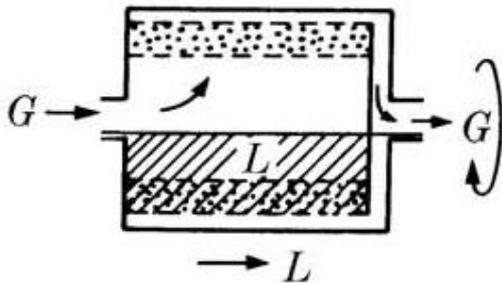
Converter



Example:  
steel production

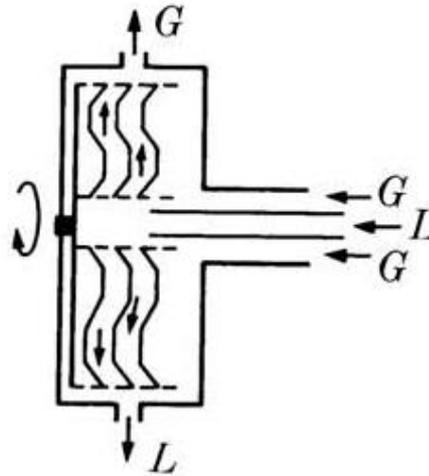
# Gas-liquid reactors<sup>[15]</sup>

Drum scrubber



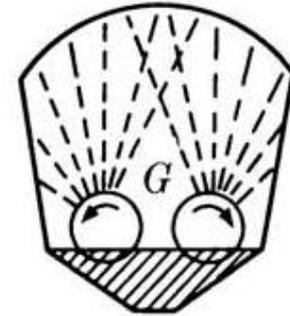
Example:  
ammonia  
scrubbing

Plate scrubber



Example:  
separation of tar  
from coke-oven gas

Rotary scrubber



Example:  
 $\text{SO}_3$  absorption

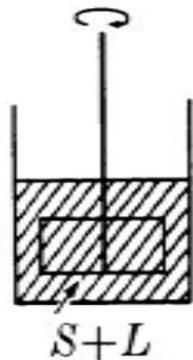
# Gas-liquid reactors

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Think other possible designs.

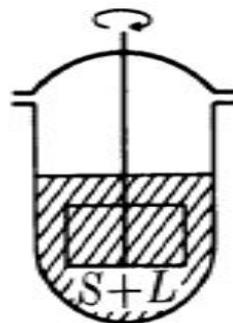
# Liquid-solid reactors<sup>[15]</sup>

Stirred-tank reactor



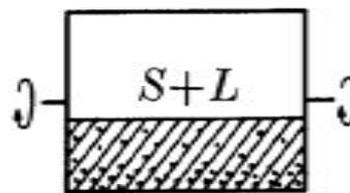
Example:  
dyeing

Autoclave



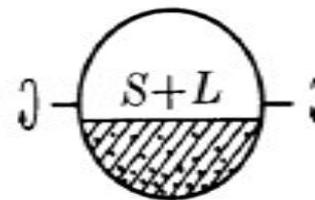
Example:  
Bayer process  
for  
 $\text{Al}(\text{OH})_3$

Rotary drum



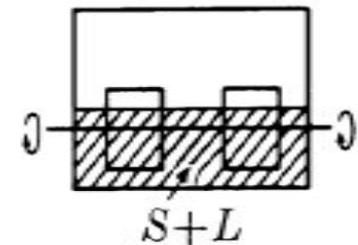
Example:  
lime  
slaking

Rotary sphere



Example:  
antimony  
from tin  
ore

Agitated drum



Example:  
ammonia  
from  
ammonium  
chloride

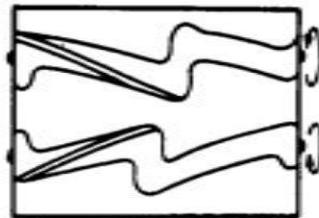
# Liquid-solid reactors<sup>[15]</sup>

Reactor with circulation



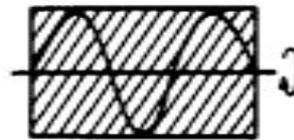
Example:  
cellulose digester

Kneader



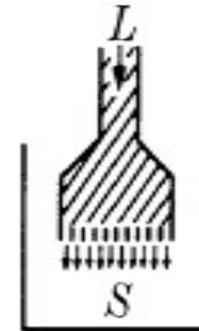
Example:  
superphosphate  
from rock  
phosphate

Screw



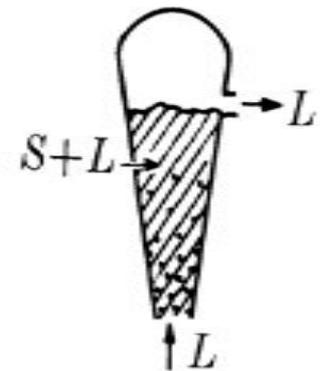
Example:  
Buna  
rubber  
polymeriza-  
tion

Spinning  
nozzle



Example:  
rayon  
production

Fluidized-bed  
reactor



Example:  
water softening

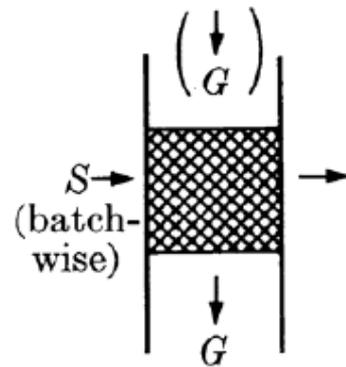
# Gas-solid reactors<sup>[15]</sup>

Reactor with fixed solids



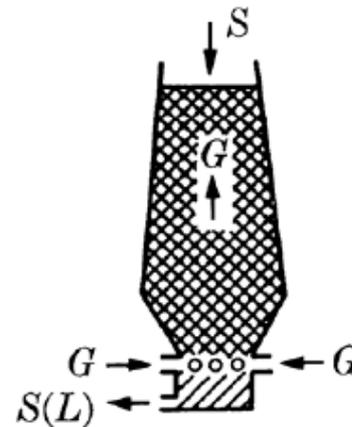
Examples:  
 $N_2 + 3H_2 \rightarrow 2NH_3$   
 (with catalyst),  
 heat regenerator  
 (with refractory  
 material)

Batch reactor



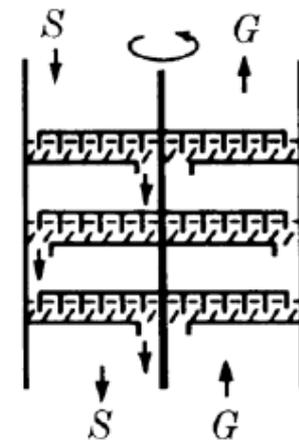
Example:  
 coking of  
 coal

Moving-bed reactor



Examples:  
 iron smelting,  
 calcination  
 of limestone

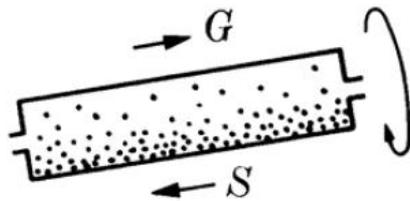
Multicompartiment reactor



Example:  
 roasting  
 of ore

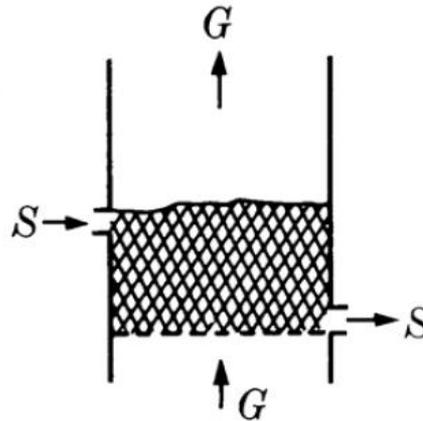
# Gas-solid reactors<sup>[15]</sup>

Rotary kiln



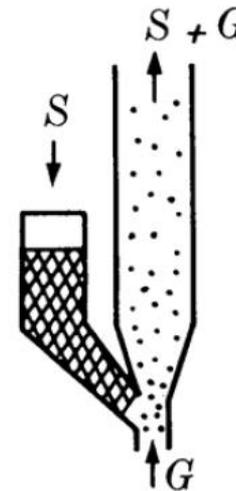
Examples:  
roasting  
of ore,  
cement  
manufacture

Fluidized-bed  
reactor



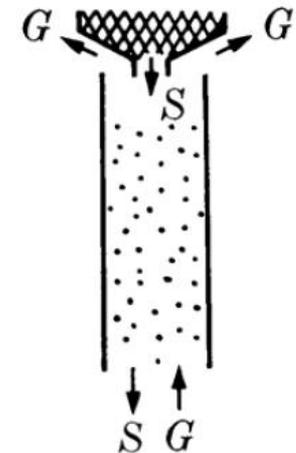
Examples:  
coal gasification,  
cracking,  
roasting  
of ore

Dilute-phase,  
cocurrent-flow  
reactor



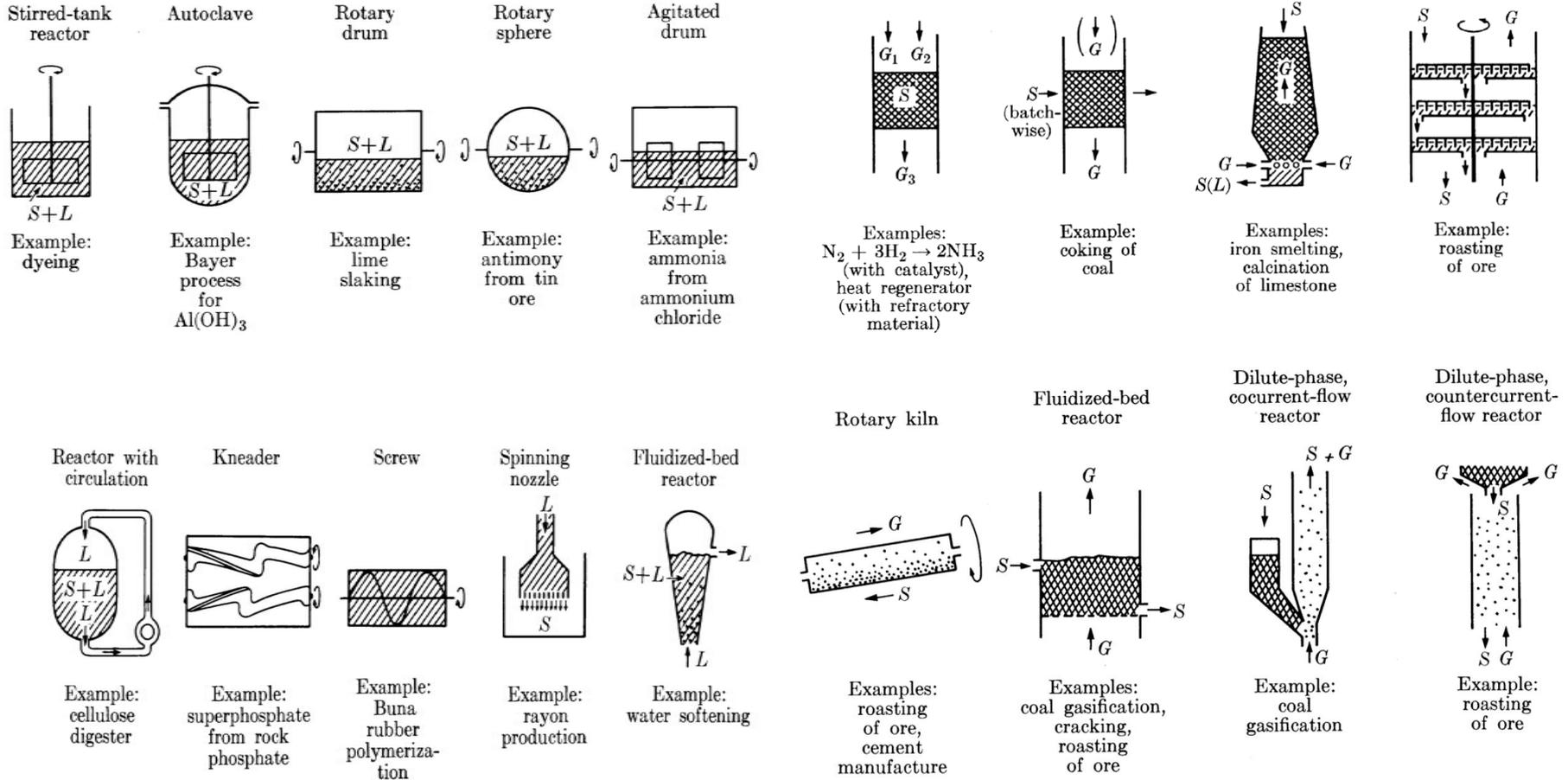
Example:  
coal  
gasification

Dilute-phase,  
countercurrent-  
flow reactor



Example:  
roasting  
of ore

# Gas-Liquid-solid reactors<sup>[15]</sup>



# Possible design of reactors

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Think other designs.

Make your own designs.

You may have a novel idea.

# Basic types of furnaces<sup>[14]</sup>

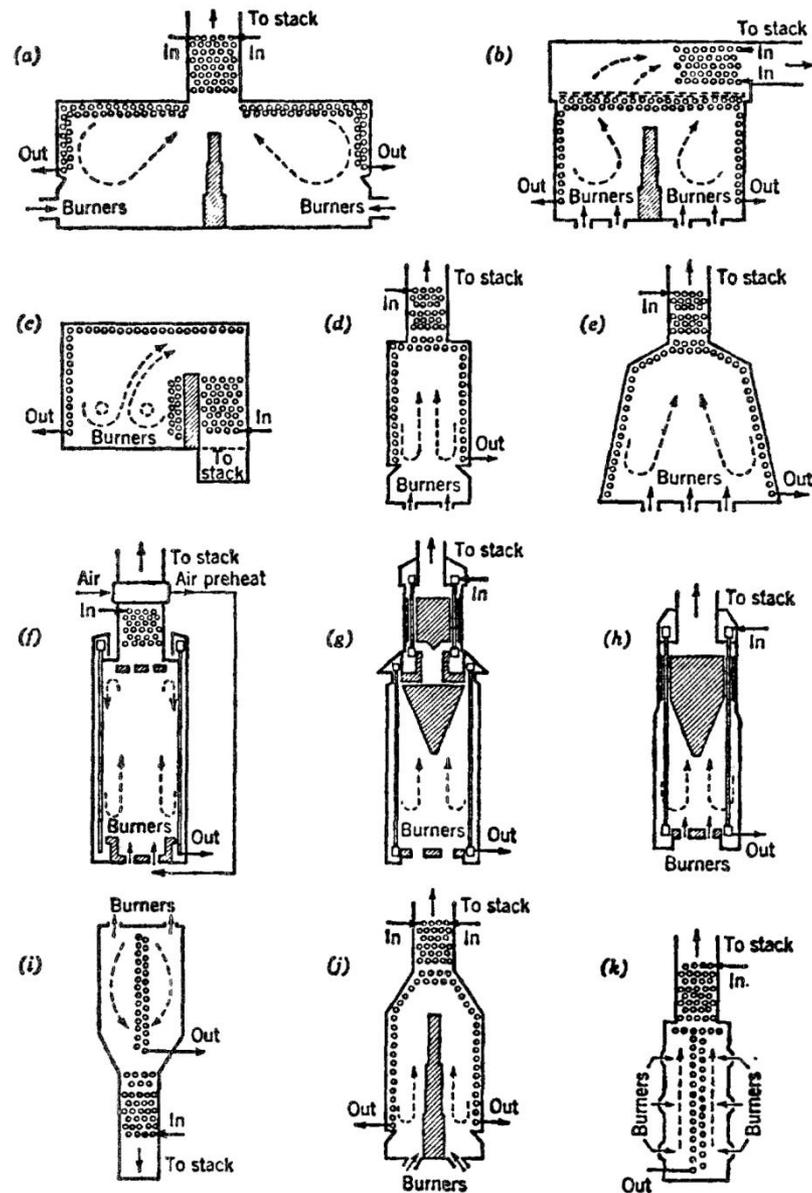


Figure 17.16. Basic types of tubular furnaces [Nelson, Petroleum Refinery Engineering, McGraw-Hill, 1958. Courtesy McGraw-Hill, New York].

# Gas-Liquid-solid reactors<sup>[14]</sup>

CODE:  Commonly used  Rarely used  Not feasible

MODE	BATCH	CONTINUOUS				
REACTOR TYPE	Tank	Tank	Tank battery		Tubular	
Flow type	Agitated	Agitated	Parallel	Counter	Parallel	Counter
Phase						
Gaseous	<input type="checkbox"/>					
Liquid	<input type="checkbox"/>					
Gas-liquid	Gas continuous	<input type="checkbox"/>				
Liquid-liquid	<input type="checkbox"/>					
Gas-solid	<input type="checkbox"/>					
Liquid-solid	<input type="checkbox"/>					
Gas-liquid-solid	<input type="checkbox"/>					
Flowsketch for the reaction $A + B \rightleftharpoons R + S$						

# Design of a fixed bed reactor

A commonly used fixed bed reactor has the following features:

- ✚ The reactor is used for a fluid-solid contact though gas-solid systems are more common.
- ✚ The solid catalyst particles are arranged randomly in a cylindrical shell or tube, where the solid particles remain fixed with respect to each other as well with respect to the reactor wall.

How will you define **moving bed reactor** and **fluidized bed reactor**?

# Design of a fixed bed reactor

- ✚ The gas or liquid flows from top to the bottom. The flow in upward direction may loosen the bed giving rise to attrition and fine particles may increase the pressure drop and may possibly be fluidized.
- ✚ Sulfuric acid production ( $\text{SO}_2$  oxidation), methanol production, ammonia synthesis, manufacture of styrene by the dehydrogenation of ethylbenzene are some of the industrial examples that require a fixed bed reactor.
- ✚ The catalytic bed may be arranged in a single shell or single shells stacked one above the other.

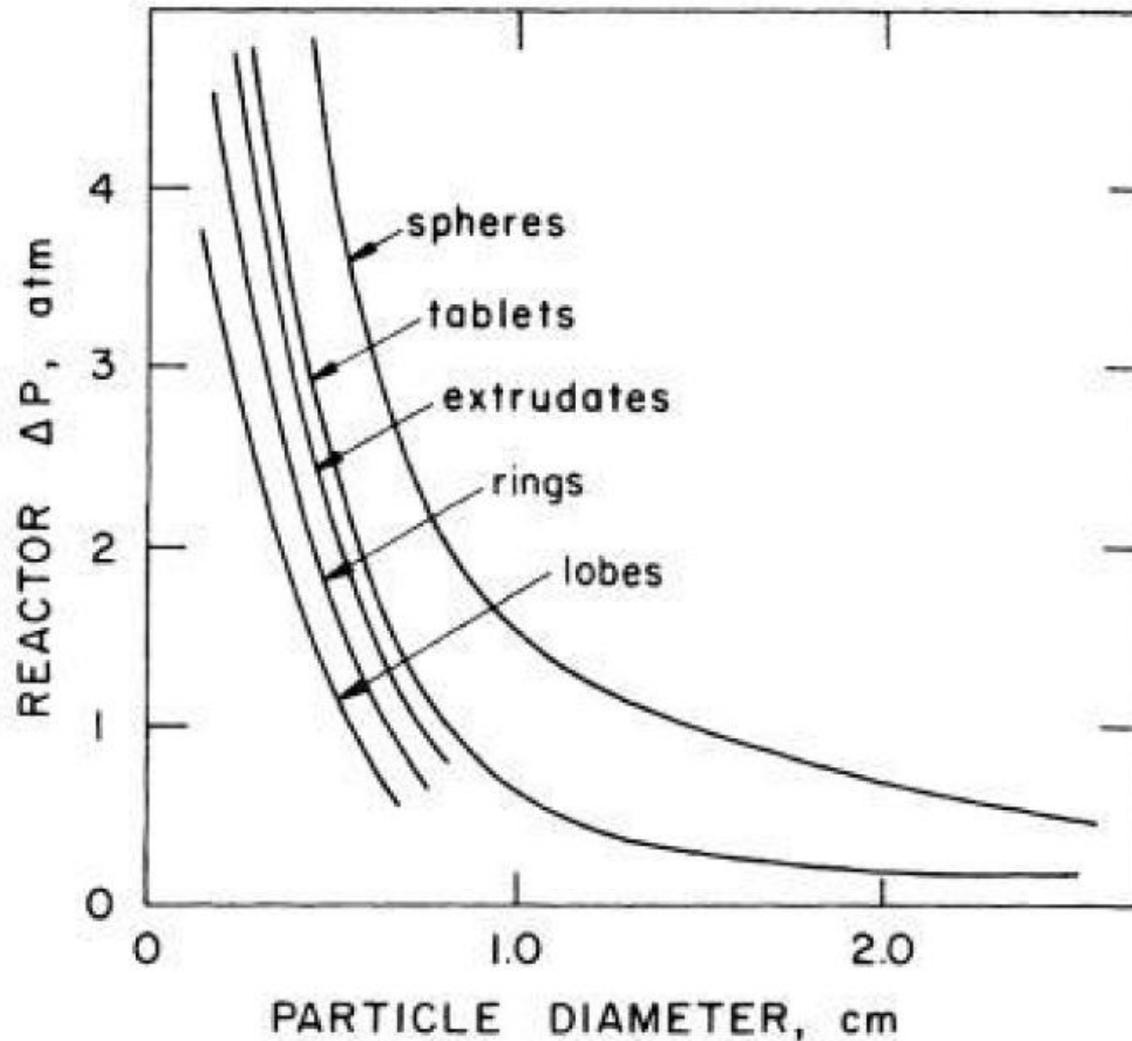
# Design of a fixed bed reactor

✚ The catalyst bed may be arranged in a multitubular geometry in which a set of tubes are placed inside a shell. This conforms to a shell and heat exchanger type assembly. The catalyst may be packed inside or outside of the tubes.

✚ A radial flow reactor may also be used where pressure drop is an issue.

✚ The usual catalyst particle size ranges between 2-6 mm. Various shapes of catalysts may be used. Spherical, solid cylindrical, hollow cylindrical (Raschig ring type), Lessing ring type, extrudates, etc., are the different kinds of shapes of catalyst that may be employed.

# Variety of catalysts: pressure drop [17]

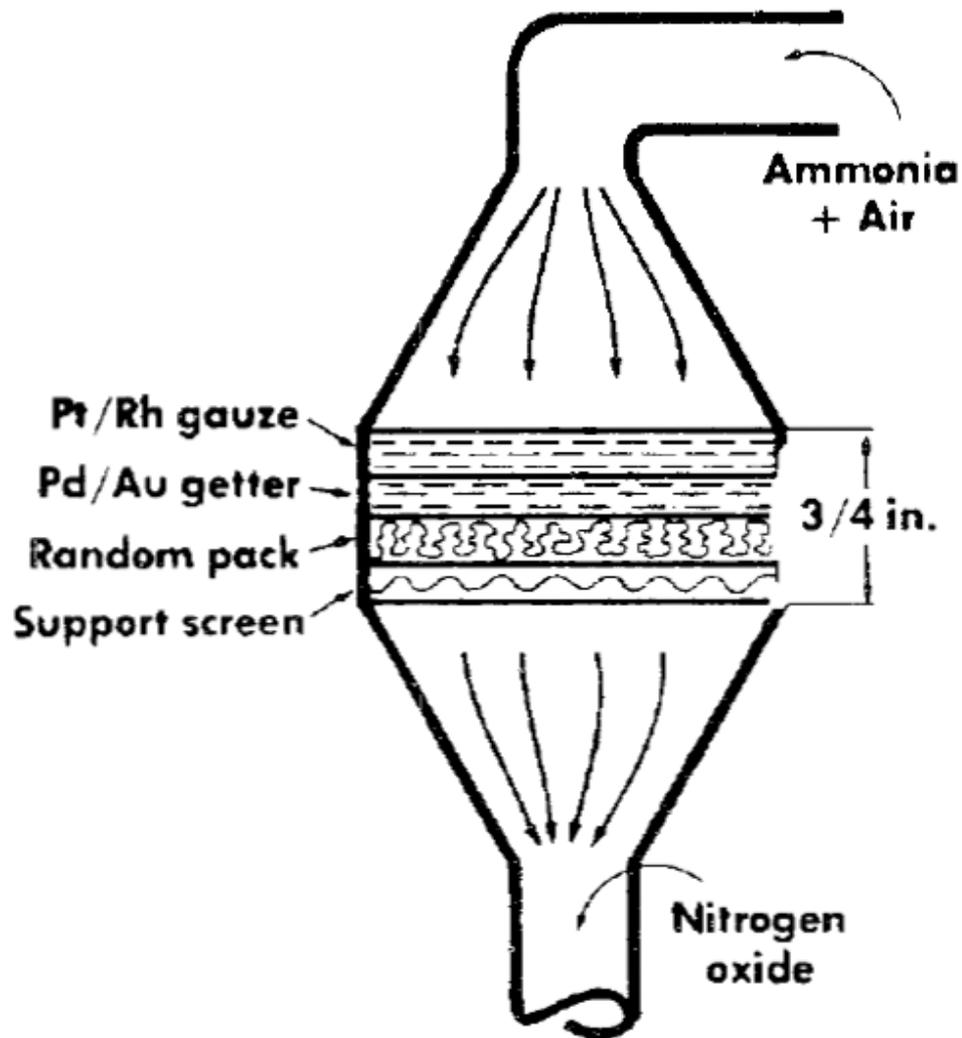


# Design of a fixed bed reactor

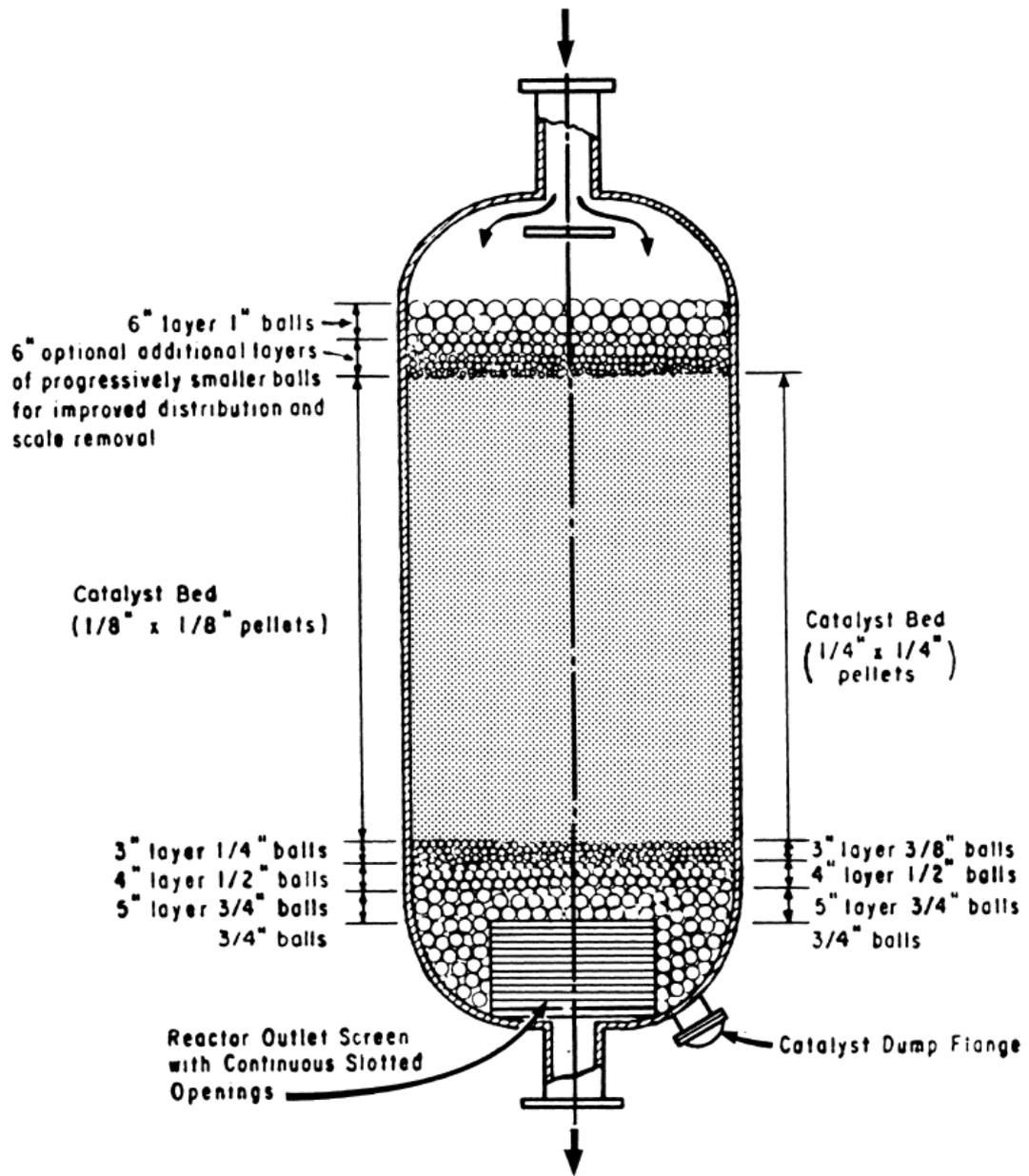
- ✦ Thermodynamics of the reaction (heat of reaction and chemical reaction equilibrium consideration)
- ✦ Reaction reversibility
- ✦ Kinetics (rate) of the given reaction
- ✦ Feed composition and product specifications
- ✦ Flow requirement
- ✦ Thermal energy requirement
- ✦ Bed arrangement
- ✦ Properties of catalytic particles and catalytic bed
- ✦ Catalyst weight (size of the reactor)
- ✦ Length to diameter ratio
- ✦ Pressure drop
- ✦ Temperature and composition distributions

One or more of these requirements may be dependent on each other.

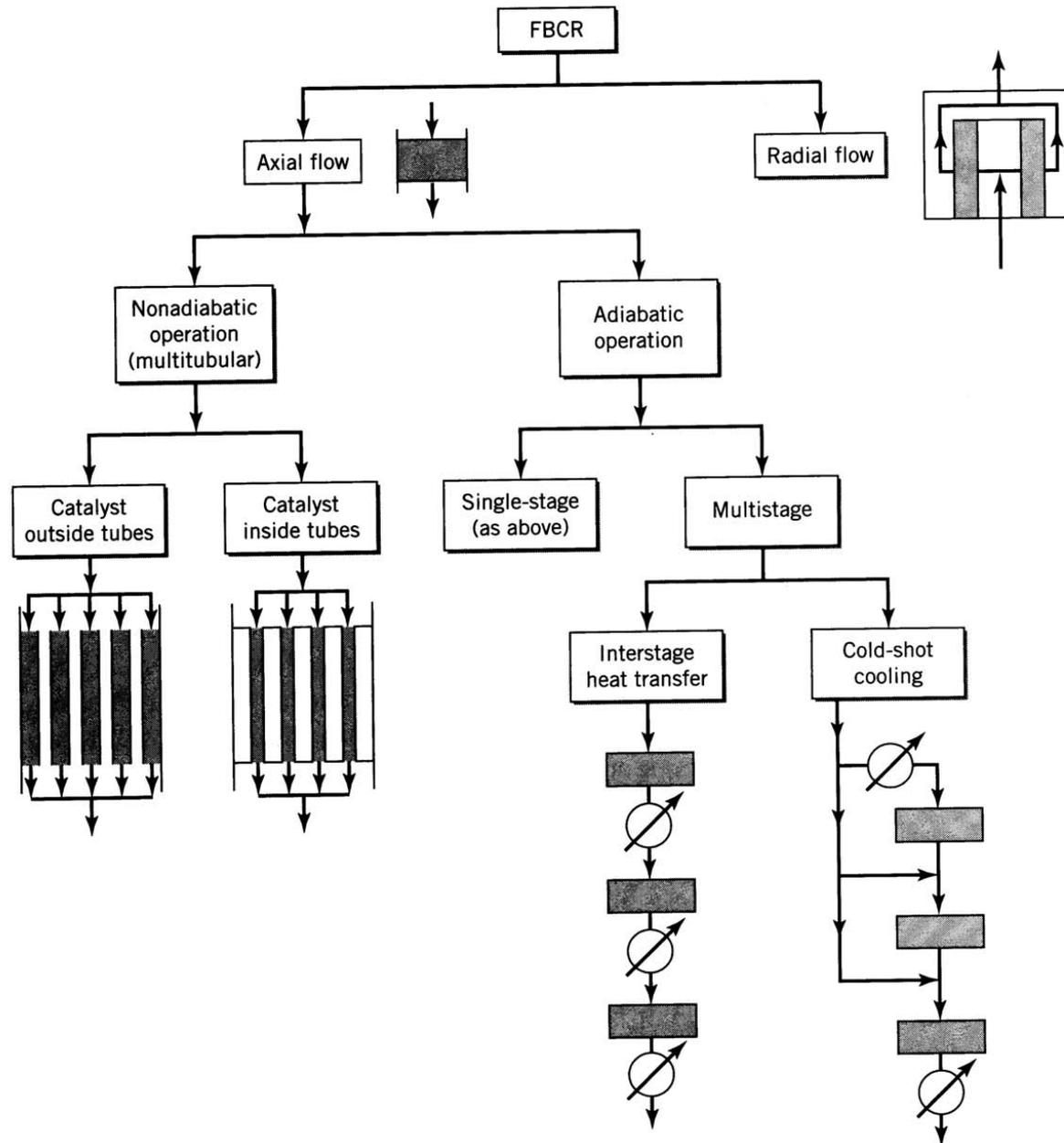
# Example fixed bed reactor<sup>[14]</sup>



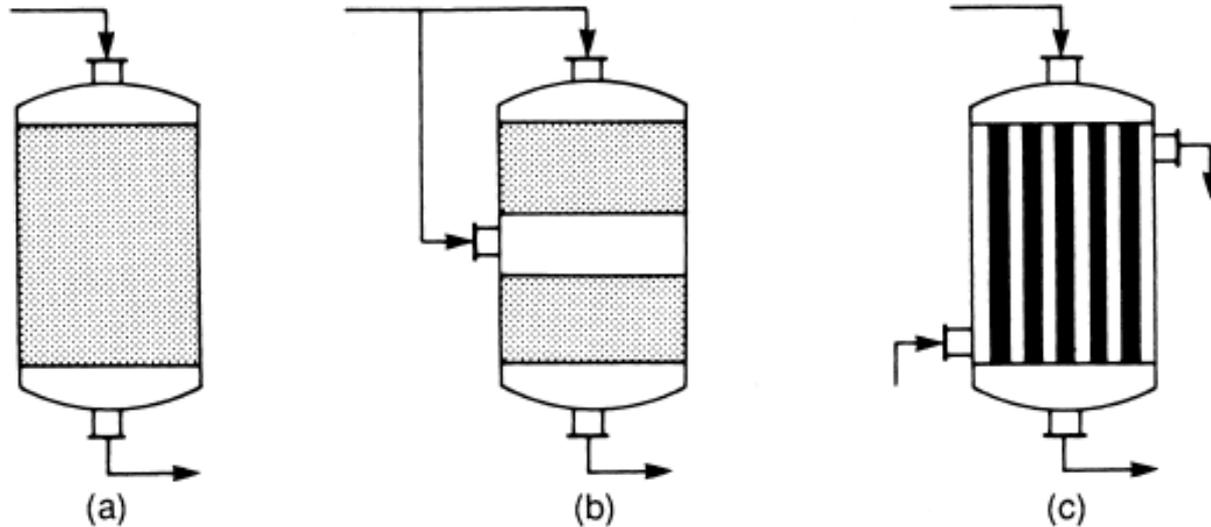
# Example fixed bed reactor<sup>[16]</sup>



# Various kinds of fixed bed reactors<sup>[10]</sup>



# Various kinds of fixed bed reactors<sup>[14]</sup>



(a) adiabatic; (b) interbed coldshot injection; (c) shell and tube;

# References

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- [16] Rase, H.F. 1990. Fixed bed reactor design and diagnostics: Gas-phase reactions, Butterworths, Boston.
- [17] Richardson